Lecture 5

Material balance in Coke making

In coke-making, it is often required to calculate the amount of coke, coke oven gas and tar produced per ton of coal. This can be done by performing elemental balance. For this purpose ash, C, N, H and O balance can be done to obtain the required information. This is illustrated by the following problem:

1. By product coke ovens are surrounded by air. There may occur leakage of air in the oven. Consider a coke-oven surrounded by moist air, (The air is at 750 mm Hg pressure and 26°C temperature). The relative humidity of air is 40%. It carbonizes coal of the composition (Wt%) C76.1, H 4.6, N2.3, S 1.9, O 2.5, H2O 6.3 and ash 6.3. The following product and by products are produced:

Product: Coke (Wt %) C 85.2, H 1.9, O 2.2, N 0.8, S 1.2 and Ash 8.7

By –product: (a) Coke oven gas (vol % dry basis)

and C6H6 1.1, C2H4 2.7, CH4 4.4, CO 1.7, CO2 1.3, H2 36.5, N2 6.9, O2 2, H2S 2.1 and NH3 1.3

(b) Tar (40 kg/ton of coal) analysis (Wt %)

C=89.4, H 4.5, N 1.1. and incombustibles Rest.

Required per ton of Coal

i. Amount of coke /ton of coal

ii. Amount of coke-oven gas

iii. fraction of S in coke and coke oven gas

iv. Amount of air leakage: The vapor pressure of moisture in air at saturation is 25.21 mmHg.

v. Calorific value in coke and coke oven gas in terms of fraction of calorific value of Coal.

Solution: Basis of calculation: 1000 kg coal

i. Amount of coke /ton of coal

Ash balance is used to determine the amount of coke. Let x kg is amount of coke.

\[
\frac{6.3 \times 1000}{100} = \frac{x \times 8.7}{100}
\]

\[
\therefore x = 724.1 \text{ kg coke Answer.}
\]
ii. Amount of coke oven gas can be calculated by performing C balance
C from coal= C in tar+ C in coke + C in Cokes oven gas

Let y kg is the amount of Cokes oven gas

\[
\frac{761}{12} = \frac{0.894 \times 40}{12} + \frac{0.852 \times 724.1}{12} + y \left[ 6 \times 0.01 + 2 \times 0.027 + 0.344 + 0.117 + 0.013 \right]
\]

By solving we get y = 15.357 kg mole

iii. Sulphur distribution

a) \( f_s \) = fraction of S in coke = \( \frac{S \text{ in coke}}{S \text{ in coal}} \) = 0.457 Ans.

b) fraction of S in coke oven gas = \( \frac{0.021 \times 15.357 \times 32}{0.019 \times 1000} \) = 0.543 Ans.

iv. To calculate amount of air leaked in to coke oven. \( N_2 \) balance is to be done. \( N_2 \) is insert.

Let Z kg mole is amount of air leaked.

In this problem air is moist. We have to find composition of moist air. It follows from Dalton’s law;

\[
P_{N_2} + p_{O_2} + p_{H_2O} = 750 \text{ mm}
\]

Where \( p \) is partial pressure.

\[
(RH)\text{Relative humidity} = \frac{p_{H_2O}}{p_{H_2O}^s} = \frac{\text{Vapour pressure of } H_2O \text{ in air}}{\text{Vapour pressure of } H_2O \text{ at saturation}}
\]

\[
P_{N_2} + p_{O_2} + RH \times p_{H_2O}^s = 750
\]

Substituting the value of RH and \( p_{H_2O}^s \), we get after simplification

\[
\therefore p_{N_2} = 584.533, p_{O_2} = 155.382 \text{ and } p_{H_2O} = 10.084
\]

\[
\therefore \text{moles of } N_2 \text{ from moist air} = \frac{548.533}{750} = 0.7794
\]

\( N_2 \) from coal+ \( N_2 \) from air = \( N \) in coke + \( N \) in tar+ \( N_2 \) in coke oven gas

\[
\frac{0.023 \times 1000}{28} + 0.7794 Z = \frac{0.8 \times 724.1}{28} + \frac{0.011 \times 40}{28} + (0.069 + 0.0065) \times 15.357.
\]
Solving: Z=20.84 kg air leaked Ans.

V. Calorific value calculation
I. Coal. First we have to convert ultimate analysis of moist coal to dry coal. (This is illustrated in Lecture 3).

Using Dulong’s formula:

\[ \text{GCV of coal} = 81 \times 81.22 + 341 \left( 4.91 - \frac{2.67}{8} \right) + 22 \times 2.03 \]
\[ = 8183.98 \text{ k cal/kg.} \]

Similarly CV of coke and tar could be calculated.

GCV of coke = 7481.72 k cal/kg.

GCV of tar = 8775.9 k cal/kg.

Calorific Value of Coke oven gas: It can be determined by adding calorific values of all combustible components of Coke oven gas.

<table>
<thead>
<tr>
<th>Combustible components Of coke oven gas</th>
<th>Heat of Combustion (k cal/kg mole)</th>
<th>Combustible components (kg mole)</th>
<th>Calorific value kcal.</th>
</tr>
</thead>
<tbody>
<tr>
<td>C\textsubscript{6}H\textsubscript{6}</td>
<td>736 \times 10\textsuperscript{3}</td>
<td>0.1689</td>
<td>124.3 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>C\textsubscript{2}H\textsubscript{4}</td>
<td>297.5 \times 10\textsuperscript{3}</td>
<td>0.4146</td>
<td>123.4 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>CH\textsubscript{4}</td>
<td>194.91 \times 10\textsuperscript{3}</td>
<td>5.2830</td>
<td>1029.67 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>CO</td>
<td>67.6 \times 10\textsuperscript{3}</td>
<td>1.796</td>
<td>121.4 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>H\textsubscript{2}</td>
<td>57.8 \times 10\textsuperscript{3}</td>
<td>5.605</td>
<td>323.97 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>H\textsubscript{2}S</td>
<td>123.96 \times 10\textsuperscript{3}</td>
<td>0.3225</td>
<td>39.98 \times 10\textsuperscript{3}</td>
</tr>
<tr>
<td>NH\textsubscript{3}</td>
<td>75.8 \times 10\textsuperscript{3}</td>
<td>0.199</td>
<td>15.13 \times 10\textsuperscript{3}.</td>
</tr>
</tbody>
</table>

Total 1778.85 \times 10\textsuperscript{3}
fraction of calorific value of coal in Coke \( f_1 \) = \( \frac{7481 \times 724.1}{8183.98 \times 1000} \) = 0.6618

fraction of calorific value of coal in tar \( f_2 \) = \( \frac{8775.9 \times 40}{8183.98 \times 1000} \) = 0.0429

fraction of calorific value of coal in coke oven gas \( f_3 \) = \( \frac{1778.85 \times 10^3}{8183.98 \times 10^3} \) = 0.2172

unaccounted calorific value of coal = 1 - (0.6618 + 0.0429 + 0.2172) = 0.0781.

This shows that 7.81\% of calorific value of coal is being utilized in raising temperatures of coke oven gas and tar to the discharge temperature.

A by-product coke-oven carbonizes coal of the composition (Wt \%) C 75.2, H 3.4, O 5.8, N 3.5, \( \text{H}_2 \text{O} \) 4.6 and ash 7.5. The Coke produced contains C 88.2\%, H 0.2\% and ash 11.6\%. Tar contains 52kg carbon. The Coke-oven gas produced analysed (vol \% dry) \( \text{CH}_4 \) 28.2, \( \text{H}_2 \), 56.4, \( \text{C}_2\text{H}_4 \) 2.2, \( \text{C}_6\text{H}_6 \) 0.8, \( \text{CO}_2 \) 1.7, \( \text{CO} \) 6.0, \( \text{O}_2 \) 0.7 and \( \text{N}_2 \) 4

Calculate \( n \) per ton of coal.

i. Amount of coke
ii. Amount of coke oven gas.
iii. Fraction of calorific value of coal (a) in coke and (b) Coke-oven gas.

**Answer:**

i. 647kg
ii. 536 m\(^3\) (1 atm, 273 K)
iii. (a) 0.63 (b) 0.34

Those interested to solve more problems, see the following book.

1. A. Butts Metallurgical problems.